
MultiFlow: A coupled balanced-force framework to solve multiphase flows in arbitrary domains

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- Multiphase flows are frequently encountered in industry and nature.



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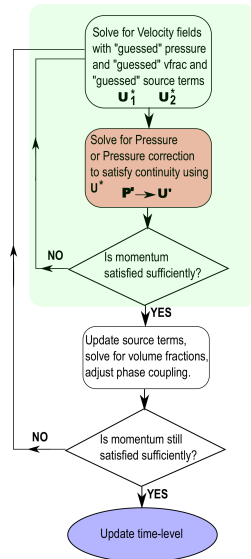
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 - ▶ etc.
- Current algorithms for multiphase flows are typically based on single phase flows.
 - ▶ They lack efficiency and robustness for multiphase flows.
- Most flows occur in complex geometries, therefore a collocated variable arrangement is more natural (in a finite volume framework).

Introduction

Incompressible Navier-Stokes equations

$$\begin{aligned}\nabla \cdot \mathbf{u} &= 0 \\ \rho \left[\frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot (\mathbf{u} \otimes \mathbf{u}) \right] &= -\nabla p + \nabla \cdot \boldsymbol{\tau} + \mathbf{s}\end{aligned}$$

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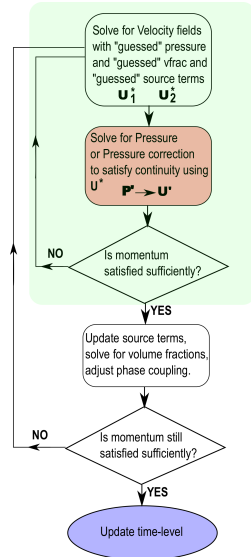


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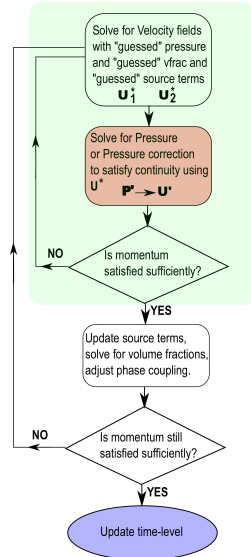


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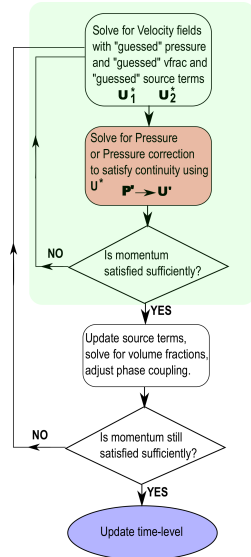


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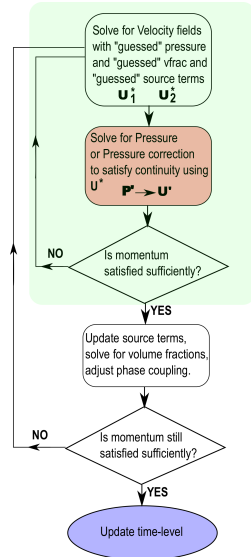


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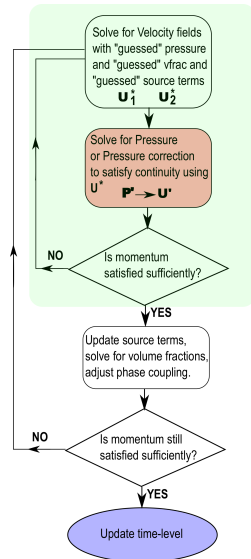


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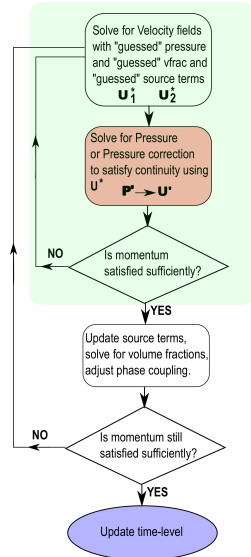
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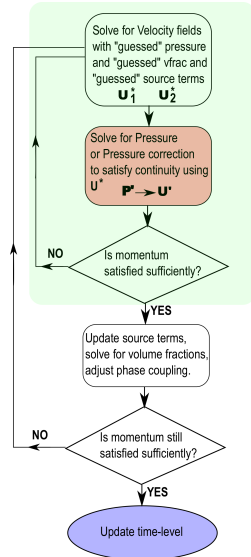
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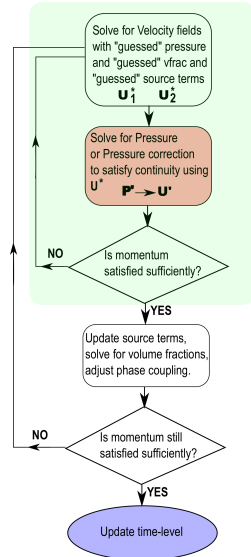
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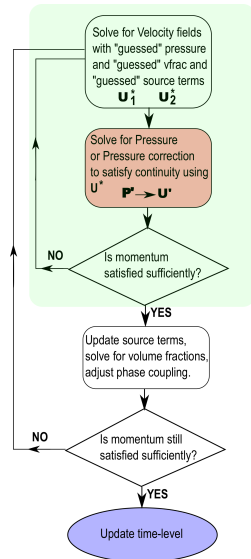
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- ▷ Difficulties arise with **large source terms**.



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 - ▷ Including pressure dependency in the continuity equation.
 - Requires a different approach to the discretisation.

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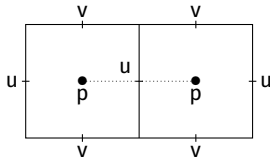
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Staggered vs. collocated discretisation

- A staggered variable storage mitigates pressure velocity decoupling.

Perot (2000), Wenneker et al (2003)

- ▷ The natural discretisation of the pressure gradient directly drives the velocity.
 - *This provides a “natural” coupling between pressure and velocity.*
- ▷ Very compact stencil for pressure.
- ▷ Preferred configuration for Cartesian grids.
 - *Used by most research codes.*
- ▷ For complex geometries ... not so simple!

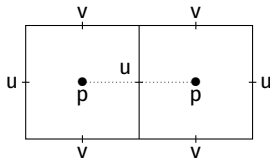


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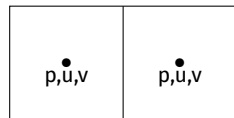
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- A colocated variable storage allows for arbitrary meshes.

- ▷ Trivial application to arbitrary meshes.
- ▷ But: naive implementation can lead to pressure-velocity decoupling.



Momentum weighted interpolation

- Introduces a pressure dependency in the continuity equation.
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- Yields a strong cell-to-cell pressure-velocity coupling.
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- The idea of Momentum Weighted Interpolation was first introduced by Rhie and Chow (1983).
- This idea has been further developed in our work for multiphase flow calculations.

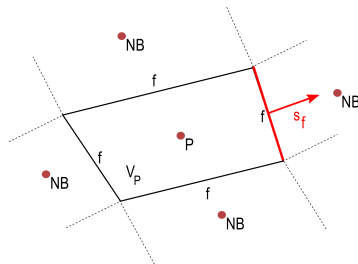
Denner & van Wachem, *Num. Heat Transfer Part B* 65-3 (2014), 218-255

Bartholomew et al., *J. Comput. Phys.* 375 (2018), 177-208

Momentum weighted interpolation

Navier-Stokes equations

$$\rho \frac{\partial u_j}{\partial t} + \rho \frac{\partial}{\partial x_i} (u_i u_j) = - \frac{\partial p}{\partial x_j} + \frac{\partial \tau_{ij}}{\partial x_i} - s_j$$
$$\frac{\partial}{\partial x_i} u_i = 0$$



Discretised Navier-Stokes equations

$$\left[\frac{\rho V_P}{\Delta t} + a_P \right] u_{j,P} = \left[\sum_{nb} a_{nb} u_{j,nb} \right] - V_P \left[\sum_{nb} b_{nb} p_{nb} + s_j \right] + \left[\frac{\rho V_P}{\Delta t} \right] u_{j,P}^O$$
$$\sum_{f=\text{faces}} u_{i,f} s_{i,f} = \sum_{f=\text{faces}} \vartheta_f = 0$$

Momentum weighted interpolation

- The net force *driving* the flow is the pressure gradient and sources,

Net driving force

$$\widetilde{\frac{\partial p}{\partial x_j}} = \left[\frac{\partial p}{\partial x_j} - s_j \right]$$

- With this, the discretised equation becomes:

Discretised Momentum equations

$$\left[1 + \frac{\rho}{\Delta t} \frac{V_P}{a_P} \right] u_{j,P} = \left\{ \frac{[\sum_{nb} a_{nb} u_{j,nb}]}{a_P} \right\} - V_P \frac{\left[\widetilde{\frac{\partial p}{\partial x_j}} \right]_P}{a_P} + \left[\frac{\rho}{\Delta t} \right]_P \frac{V_P}{a_P} u_{j,P}^O$$

Momentum weighted interpolation

- Using the following

Abbreviations

$$c_P = \frac{\rho}{\Delta t} \quad d_P = \frac{V_P}{a_P} \quad \widetilde{u}_{j,P} = \left\{ \frac{[\sum_{nb} a_{nb} u_{j,nb}]}{a_P} \right\}$$

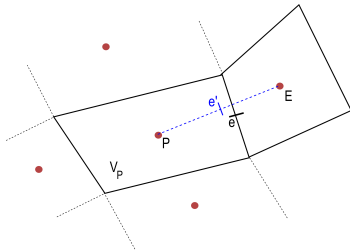
- The discretised equation becomes

Momentum equations

$$[1 + c_P d_P] u_{j,P} = \widetilde{u}_{j,P} - d_P \left[\frac{\partial p}{\partial x_j} \right]_P + c_P d_P u_{j,P}^O$$

Momentum weighted interpolation

- Such a discretised equation for cell E can also be written out,



- then an *analogous* equation for location e' can be constructed:

Momentum equation at e'

$$[1 + c_{e'} d_{e'}] u_{j,e'} = \widetilde{u_{j,e'}} - d_{e'} \left[\frac{\partial p}{\partial x_j} \right]_{e'} + c_{e'} d_{e'} u_{j,e'}^O$$

Momentum weighted interpolation

- Writing out the terms which are interpolated to e' ,

U velocity at e'

$$u_{j,e'} = \frac{u_{j,P} + u_{j,E}}{2} - \frac{d_{e'}}{[1 + c_{e'} d_{e'}]} \left(\left[\frac{\partial p}{\partial x_j} \right]_{e'} - \frac{1}{2} \left[\frac{\partial p}{\partial x_j} \right]_P - \frac{1}{2} \left[\frac{\partial p}{\partial x_j} \right]_E \right) \\ + \frac{c_{e'} d_{e'}}{[1 + c_{e'} d_{e'}]} \left(u_{j,e'}^O - \frac{1}{2} u_{j,P}^O - \frac{1}{2} u_{j,E}^O \right)$$

- There are various ways to go from e' to e , for instance

From e' to e

$$u_{j,e} = u_{j,e'} + \frac{\overline{\partial u_j}}{\partial x_i}_{e'} (x_{i,e'} - x_{i,e})$$

- Now there is an *analogous analytical* expression for the face velocity which depends on pressure.

Momentum weighted interpolation

- This expression can be directly used in the continuity equation.
- $\vartheta = \mathbf{u}_f \cdot \mathbf{n}_f$, the flux at the face, is only needed.
 - ▷ For a steady-state situation, the expression for ϑ *does not depend on the time-step*.
 - ▷ The pressure terms are analogous to $\Delta^2 \frac{\partial^3 p}{\partial x^3}$.
This is similar to a filter, which converges to zero with the same order as the discretisation.

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- The expression can be used in a *finite volume* framework for any type of cell.

Momentum weighted interpolation

- Advected variables discretised with TVD schemes
Denner & van Wachem, *J. Comput. Phys.* 298 (2015), 466
- Transient terms discretised with backward Euler scheme
 - ▶ First-order or second-order backward Euler scheme
 - ▶ Same scheme applied for all transient terms

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- Advecting velocity evaluated with momentum-weighted interpolation

Bartholomew et al., *J. Comput. Phys.* 375 (2018), 177

- ▶ Pressure-velocity coupling for low-Mach flows
- ▶ Source terms require special reconstruction to ensure force balance

Advecting velocity

$$\vartheta_f = \overline{\mathbf{u}}_f \mathbf{n}_f - \hat{d}_f \left(\nabla p_f - \overline{\nabla p_f} \right) \mathbf{s}_f + \hat{d}_f \left(\mathbf{S}_f - \overline{\mathbf{S}}_f \right) \mathbf{s}_f + \hat{d}_f \frac{\rho_f}{\Delta t} \left(\vartheta_f^O - \overline{\mathbf{u}}_f^O \mathbf{n}_f \right)$$

Solution procedure

- Governing flow equations solved in single equation system
 - ▶ Robust even for large pressure or density discontinuities
- No underrelaxation necessary
- Solved using the PETSc library
 - ▶ *Block-Jacobi* preconditioner
 - ▶ *BiCGStab* solver

Linear system of equations

$$\begin{pmatrix} A_u & A_v & A_w & A_p & 0 \\ B_u & B_v & B_w & B_p & 0 \\ C_u & C_v & C_w & C_p & 0 \\ D_u & D_v & D_w & D_p & 0 \\ E_u & E_v & E_w & E_p & E_h \end{pmatrix} \cdot \begin{pmatrix} \phi_u \\ \phi_v \\ \phi_w \\ \phi_p \\ \phi_h \end{pmatrix} = b$$

Momentum x
Momentum y
Momentum z
Continuity
Energy

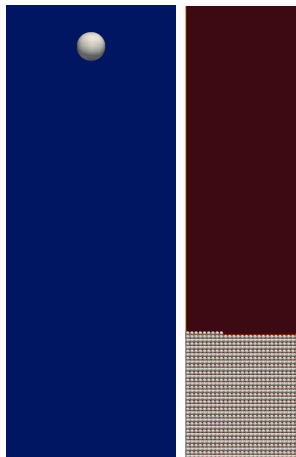
History

- Three versions of *MultiFlow*:

- ▶ All versions are based around the structure of PETSc KSP Solver, Vec, Ghost update, etc.
- 1. ***MultiFlow 1*** (since 2004)
Block structured, static mesh, “one iteration per timestep”.
 - ▶ based on multiple interconnected DMDA structures
 - ▶ uses PETSc binary file format
 - ▶ translation to/from VTK done externally
- 2. ***MultiFlow 2*** (since 2013)
Polyhedral, static mesh.
 - ▶ in-house mesh handling routines
 - ▶ partitioning with Parmetis
 - ▶ HDF5 file format (directly read by Paraview with XDMF reader)
- 3. ***MultiFlow 3*** (since 2019)
Unstructured/block structured/polyhedral, adaptive mesh.
 - ▶ Mesh handling based on DMPlex routines.
 - ▶ Adaptive refinement based on DMForest/p4est framework.

Examples of applications

Fully resolved particulate flows: IBM simulation



- Conducted in *MultiFlow 2*.
- Solid bodies modelled with IBM.
- $\mathcal{O}(10^3)$ particles.
- No-slip condition enforced with momentum sources in the region surrounding the moving bodies.
- Fully resolved particulate flows but ...very expensive!
 - ▷ Motivation for *MultiFlow 3*.

Examples of applications

Large scale fluidised bed: Euler-Lagrange simulation



- Conducted in *MultiFlow 1*.
- $\mathcal{O}(10^6)$ particles.
- Flow at the scale of the Lagrangian point particles is not resolved.
- Flow and particles are coupled via momentum transfer and volume fraction contribution.
- Individual particle motion solved separately within overlapping Cartesian mesh.

Examples of applications

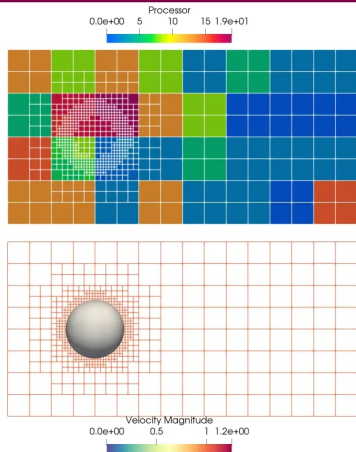
Atomising swirling spray



- Conducted in *MultiFlow 2*.
- $\mathcal{O}(10^7)$ mesh cells.
- But resolution of all scales would require (much) larger mesh!
 - ▷ Motivation for *MultiFlow 3*.

Examples of applications: MF3

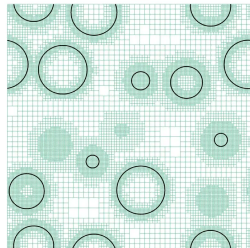
Micro-scale particle laden flow



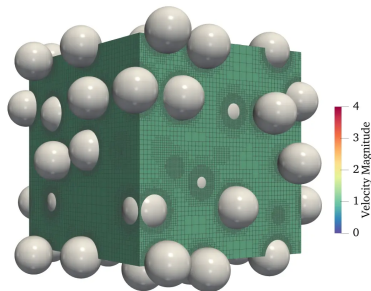
- Conducted in our new *MultiFlow 3*!
- Increasing of resolution where needed with p4est.
- Refinement is based on vorticity.

Examples of applications: MF3

Micro-scale particle laden flow



$t = 0.00 \text{ U/L}$



- Conducted in *MultiFlow 3*.
- Moving to $\mathcal{O}(10^3)$ particles and $\mathcal{O}(10^7)$ mesh cells.

MultiFlow 3: implementation

Specifications

We aim to have a coupled framework that:

- solves the (in)compressible Navier-Stokes equations in the presence of large source term and volume fraction gradients,
- is designed for arbitrary computational domains,
- can adapt the mesh where resolution is needed
(e.g. at the interface between two fluids, near an immersed boundary)
- accounts for the specificities of multiphase flow modelling

Used frameworks:

- the DMPlex routines/framework
- the DMForest/p4est framework
- the I/O routines for mesh and data

MultiFlow 3: implementation

DMPlex usage

1. For the “coupled” Vector, we create a `DMPlexCreateSection` with ≥ 4 fields.
2. For the other Vectors, we copy the `DMPlexCreateSection` and set fields to 1.
3. If necessary, we couple the `DMPlex` object to the `DMForest` object with `DMConvert`.
4. For efficiently tracking particles or interfaces, we use a `DMDA` “particle-mesh”.

MultiFlow 3: implementation

Challenges

- We are not computer scientists, and it is hard to understand the details of `DMPlex`
- As we do our own discretisation, some `DMPlex` frameworks are superfluous, but still need to be dealt with (e.g., the FE discretisation object).
- Some `DMPlex` implementations do not match our needs, e.g. HDF-5 output and `DMPlexCreateBoxMesh`.
- We have had to implement our own AMR-related routines for:
 - ▶ Computing and storing geometric mesh properties.
 - ▶ Interpolating from coarse to fine grids.
 - ▶ Handling hanging-nodes in the context of finite-volumes.
- We are struggling with the restart of AMR simulations.
- There is a bug in the combination of `DMPlex`/`P4est` for periodic meshes.

MultiFlow 3: implementation

More details

- Bartholomew, P., Denner, F., Abdol-Azis, M.H., Marquis, A., van Wachem, B., 2018. Unified formulation of the momentum-weighted interpolation for collocated variable arrangements. *Journal of Computational Physics* 375, 177-208.
- Denner, F., Evrard, F., van Wachem, B., 2020. Conservative finite-volume framework and pressure-based algorithm for flows of incompressible, ideal-gas and real-gas fluids at all speeds. *Journal of Computational Physics* 409, 109348.
- Evrard, F., Denner, F., van Wachem, B., 2020. Euler-Lagrange modelling of dilute particle-laden flows with arbitrary particle-size to mesh-spacing ratio. *Journal of Computational Physics* 8, 100078.
- Cheron, V., Evrard, F., van Wachem, B., 2023. A hybrid immersed boundary method for dense particle-laden flows. *Computers & Fluids* 105892.
- <https://www.mvt.ovgu.de/Publications.html>